

Effect the Dissociation of H₂O and CO₂ on Adiabatic Flame Temperature

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Abstract

In this study a theoretical model was accredited to show the effect of dissociation phenomenon on adiabatic flame temperature. CH₄, C₂H₆, C₃H₈ and C₄H₁₀ as gases fuel, global reaction and a thermodynamics analysis were dependent in this model to analysis a combustion to evaluated adiabatic flame temperature. Four cases are studied no dissociation, only H₂O dissociation, only CO₂ dissociation and both H₂O and CO₂ dissociation together. The results show that with dissociation adiabatic flame temperature will be decreased and the bigger effect on adiabatic flame temperature when only CO₂ dissociation. Also the effect range of equivalence ratio on dissociation phenomenon was from 0.9 to 1.1

Keyword: combustion, adiabatic flame temperature, dissociation

1. Introduction:

Combustion is one of the complex subjects that include preliminary such disciplines as physics, chemistry, thermodynamics and fluid mechanics. Combustion has a wide diversity of uses and it is used for energy's production in power plants, gas turbines and engines. The very important index in combustion is flame temperature. If it's measured at adiabatic conditions, it will be called adiabatic flame temperature. Almost it's calculated using thermodynamic analysis. There are several parameters that's effect on the value of adiabatic flame temperature such as type of fuel, initial temperature for unburned mixture, equivalence ratio ...etc.

V. Maaren and et al [1] are calculated flame temperature for flat flam burner. A relation between burnt gases temperature and the measuring burner plate temperature distribution was developed to calculate flame temperature.

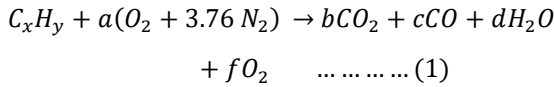
They show net heat transfer from gases to plate content heat loss from flame and heat gain by burnt gases. In other hand M. Lalovic and et al [2] are study the combustion conditions for two gaseous (natural gas and mixture of gases) fuels to show the effect of change of excess air ratio values, air preheating temperature and oxygen content in air on flame temperature. They show in their results that with increasing air preheating temperature, the flame

temperature increasing too. C. K. Liu and et al [3] are numerically study the phenomenon of superadiabatic flame temperature, the structure of planar freely propagating premixed flames of mixtures of CH₄/air, CH₄/O₂, C₂H₂/H₂/O₂, C₂H₄/O₂, C₃H₈/O₂ and H₂/O₂ was computed. Their study is perhaps superadiabatic temperatures occur only in hydrocarbon flames when the equivalence ratio of the mixture is greater than a critical value, but not in hydrogen flames. L.H. Liu and J. Jiang [4] have determined an inverse analysis for the reconstruction of temperature profile in axisymmetric free flames from the knowledge of the outgoing emission and transmission radiation intensities. Their results show that the temperature profiles can be estimated accurately, even with noisy data. Law and et al [5] are a theoretically studied adiabatic flame temperature for hydrocarbon air mixture, a water – gas shift equilibrium and dissociation of H₂O and CO₂ were studied as a parameters effect on adiabatic flame temperature. They results show the peak adiabatic flame temperature was shifted to rich side. I see that more study about effect of dissociation phenomena on adiabatic flame temperature must be done, therefor in this study four case no dissociation, only H₂O dissociation, only CO₂ dissociation and both H₂O and CO₂ dissociation together for CH₄/ C₂H₆/

C₃H₈ and C₄H₁₀ air mixture over a wide range (from 0.7 to 1.2) of equivalence ratio will be study.

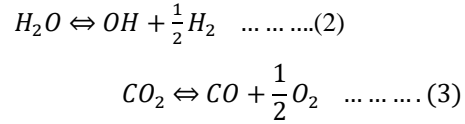
2. Theory

In this research some of assumption taken as to simplify the problem, combustion occurs at a constant pressure (atmospheric pressure), the reactants and products each form ideal gases mixture, and the reaction balance for combustion one mole of fuel expressed as [6]:

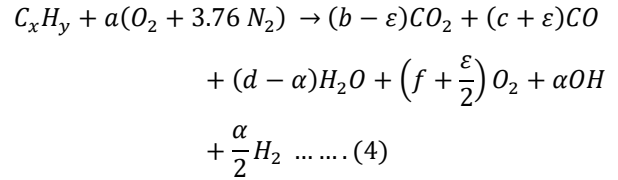


Where lean combustion, there is found oxygen in products, but for rich combustion a CO found in products, while in stoichiometry condition both are not found in products. To study the effect of dissociation on adiabatic

flame temperature only H2O and CO2 assuming that will be dissociate in products as the two reactions below [2]:



The two reversible reaction above added to the reaction of oxidizer of fuel (equation 1) yield



Where ε and α are the amount that dissociate from CO₂ and H₂O respectively and the constants of equilibrium for the two reversible reactions can be evaluated from table below:

Table (1) the logarithm of constant equilibrium for reaction 2 and 3 [2]

T(K)	H ₂ O → OH + 1/2 H ₂	CO ₂ → CO + 1/2 O ₂	T(K)	H ₂ O → OH + 1/2 H ₂	CO ₂ → CO + 1/2 O ₂	T(K)	H ₂ O → OH + 1/2 H ₂	CO ₂ → CO + 1/2 O ₂
298.15	-45.10	-45.05	1400	-6.996	-6.004	2600	-2.043	-1.194
300	-45.08	-44.74	1500	-6.280	-5.315	2700	-1.829	-0.995
400	-33.48	-32.43	1600	-5.654	-4.711	2800	-1.631	-0.813
500	-25.09	-25.03	1700	-5.102	-4.175	2900	-1.446	-0.646
600	-21.16	-20.10	1800	-4.611	-3.697	3000	-1.273	-0.491
700	-17.64	-16.57	1900	-4.172	-3.268	3100	-1.111	-0.347
800	-15.00	-13.92	2000	-3.777	-2.879	3200	-0.960	-0.208
900	-12.95	-11.86	2100	-3.419	-2.527	3300	-0.818	-0.073
1000	-11.31	-10.21	2200	-3.094	-2.207	3400	-0.684	0.062
1100	-9.922	-8.843	2300	-2.797	-1.917	3500	-0.553	0.202
1200	-8.784	-7.739	2400	-2.525	-1.652			
1300	-7.821	-6.802	2500	-2.274	-1.412			

The total number of moles present at equilibrium is depends on case of study.

For no dissociation the total mole of products calculated as:

$$Nt_1 = b + c + d + f \dots \dots \dots (5)$$

For only H2O dissociation, it is written as:

$$Nt = Nt_1 + 0.5\alpha \dots \dots \dots (6)$$

For only CO2 dissociation, it is written as:

$$Nt = Nt_1 + 0.5\epsilon \dots \dots \dots (7)$$

For both H2O and CO2 are dissociation together, it is written as:

$$Nt = Nt_1 + 0.5(\alpha + \epsilon) \dots \dots \dots (8)$$

The partial pressure for each component, p_i , may be expressed in terms of the mole fraction and the total pressure p (total pressure assuming constant and equal atmospheric pressure).

The partial pressure of species can be written as [8]:

$$p_{CO_2} = \frac{(b - \varepsilon)}{Nt} \quad \dots \dots \dots (9)$$

$$p_{CO} = \frac{(c - \varepsilon)}{Nt} \quad \dots \dots \dots (10)$$

$$p_{H_2O} = \frac{(d - \alpha)}{Nt} \quad \dots \dots \dots (11)$$

$$p_{O_2} = \frac{(f + \frac{\varepsilon}{2})}{Nt} \quad \dots \dots \dots (12)$$

$$p_{OH} = \frac{(\alpha)}{Nt} \quad \dots \dots \dots (13)$$

$$p_{H_2} = \frac{(\frac{\alpha}{2})}{Nt} \quad \dots \dots \dots (14)$$

Since the total pressure is 1 atm, the equilibrium constant, (KP1) for reaction given by equation (2) can be expressed as:

$$K_{p1} = \frac{\alpha \sqrt{\frac{(\frac{\alpha}{2})}{Nt}}}{(d-\alpha)} \quad \dots \dots \dots (15)$$

And the equilibrium constant, (KP2) for reaction given by equation (3) can be expressed as:

$$K_{p2} = \frac{(c - \varepsilon) \sqrt{\frac{(f + \frac{\varepsilon}{2})}{Nt}}}{(b - \varepsilon)} \quad \dots \dots \dots (16)$$

Adiabatic flame temperature:

Adiabatic flame temperature refers to the temperature that could be attained by the products of combustion when the combustion reaction is carried out in limit of adiabatic operation of combustion chamber. Limit of adiabatic operation of combustion chamber means that in the absence

of work, kinetic and potential energies the energy released during combustion shall be carried by the combustion products with minimum or no heat transfer to surroundings. This is the maximum temperature which can be attained in a combustion chamber and is very useful parameter for designers. Actual temperature shall be less than adiabatic flame temperature due to heat transfer to surroundings, incomplete combustion and dissociation etc.

The adiabatic flame temperature can be determined by use of the conservation of energy principles. To illustrate the procedure, let us suppose that the combustion air and the combustion products each form ideal gas mixtures. Then, with the other assumptions stated above, the energy rate balance on per mole of fuel basis, then:

$$\sum_P n_e \bar{h}_e = \sum_R n_i \bar{h}_i \quad \dots \dots \dots (17)$$

Where i denotes the incoming fuel and air streams and e the exiting combustion products.

But the enthalpy can be expressed as [6]:

$$\bar{h}_e = (\bar{h}_f^o + \Delta \bar{h})_e \quad \text{and} \quad \bar{h}_i = (\bar{h}_f^o + \Delta \bar{h})_i \quad \dots \dots \dots (18)$$

Substitute in equation 12 yield:

$$\sum_P n_e (\bar{h}_f^o + \Delta \bar{h})_e = \sum_R n_i (\bar{h}_f^o + \Delta \bar{h})_i \quad \dots \dots \dots (19)$$

Re-arrangement equation 14 yield:

$$\sum_P n_e (\Delta \bar{h})_e = \sum_R n_i (\Delta \bar{h})_i + \sum_R n_i (\bar{h}_f^o)_i - \sum_P n_e (\bar{h}_f^o)_e \quad \dots \dots \dots (20)$$

The heat of combustion can be defined as [7, 6]:

$$Q = \sum_R n_i (\bar{h}_f^o)_i - \sum_P n_e (\bar{h}_f^o)_e \quad \dots \dots \dots (21)$$

Heat of combustion consider very important factor effect on adiabatic flame temperature, with increasing heat

of combustion adiabatic flame temperature will be increased too.

And enthalpy of species i expressed as:

$$(\Delta \bar{h})_i = \int_{T_o}^{T} c_p dT \quad \dots \dots \dots (22)$$

Substitute equations 16 and 17 in equation 15 and integrated it from To (298K) to adiabatic condition in products side and to initial temperature for reactants side yeild :

$$\begin{aligned} \sum_P n_e \left(\int_{T_o}^{T_{adi}} c_p dT \right)_e \\ = \sum_R n_i \left(\int_{T_o}^{T_{in}} c_p dT \right)_i \\ + Q \quad \dots \dots \dots (23) \end{aligned}$$

The specifice heat at constant prussure for spices taken as [6]:

$$c_p = a_o + a_1 T + a_1 T^2 + a_3 T^3 \quad \dots \dots \dots (24)$$

The cofficent ao , a1, a2 and a3 are constant. The equation (18) can be solved for unknown Tadi.,(adiabatic flame temperature) by using Newton Raphson Method.

3. Results:

The phenomenon of dissoication is consideration endothermic reaction, therfor the combustion with dissociaton will be resulted to reduce in adiabatic flame temperature. This actuality was shown by Desmond E. Winterbone [7],where he was motioned the effect of dissociation is to reduce the tmperature of products after combustion. A figure (1), as cited in refrence [7] show the internal energy - temperature digram for combustion both with and without dissociation. This turn, reduces the amount of energy that can be drwon from the combustion process and reduces the work output of engines. In figure (2) the adiabatic flame temperature was ploted with equivalence ratio for methan, ethan, probane and butane fuels. In this figure can be noted the adiabatic flame temperature was approximately have same values along the wide range of equivalence ratio (from 0.7 to 1.3) except at stoichomatry value there are different in its values.

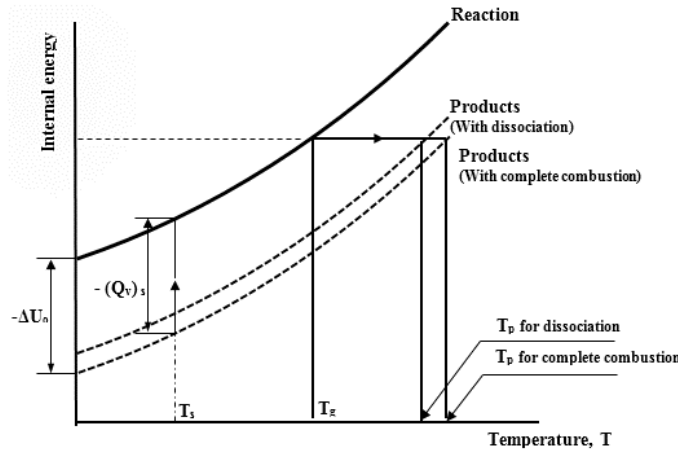


Figure (1) internal energy - temperature diagram for combustion both with and without dissociation

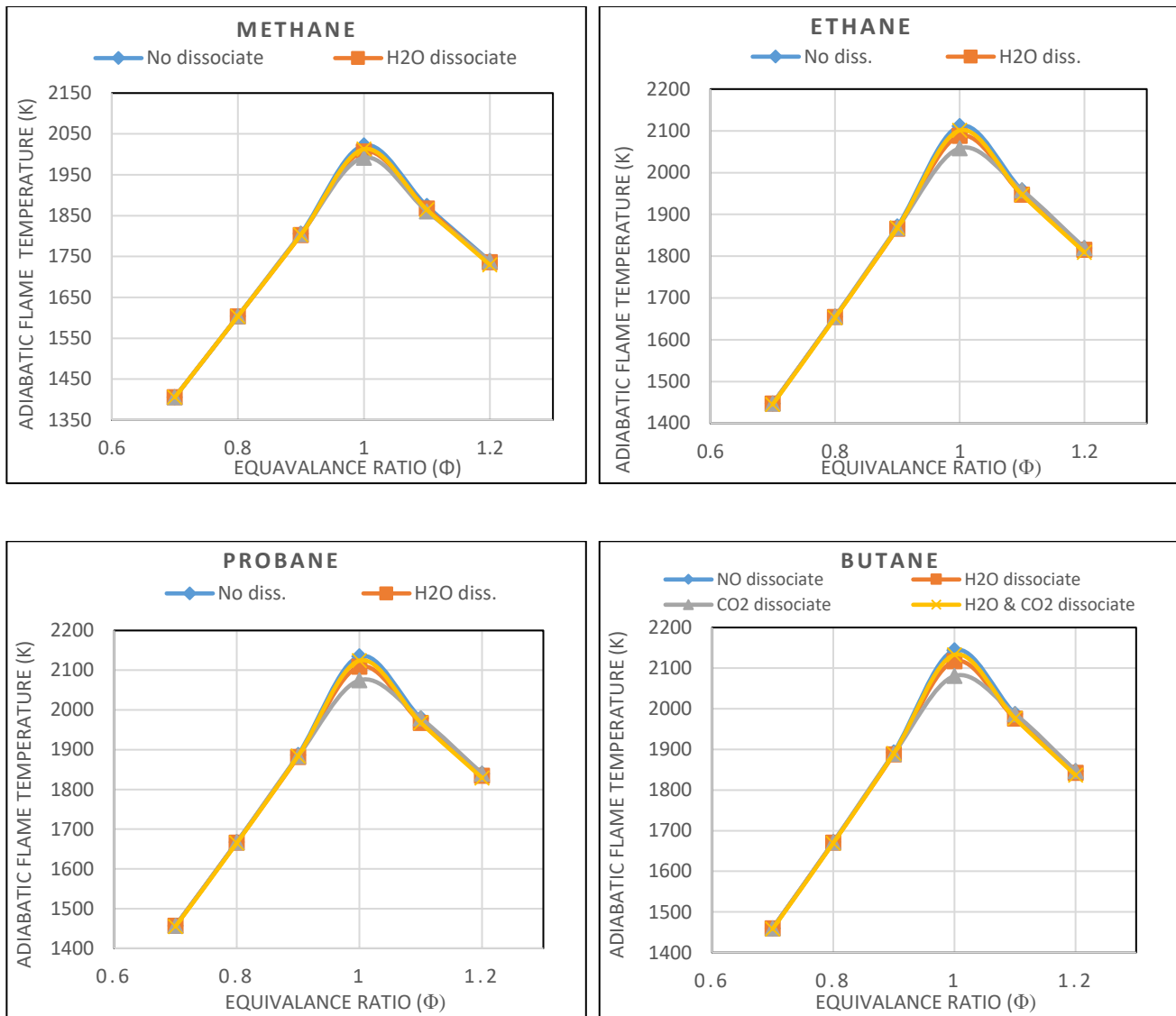


Figure (2) adiabatic flame temperature variation with equivalence ratio

The amount of dissociation depends on the temperature and it will be increased when temperature increasing too, due to the equilibrium constants for reversible reactions 2 and 3 are increasing at high temperature as shown in table 1. The dissociation is significant at temperature higher than 1500K as cited in reference [8]. Therefore, in this study, the results will be taken and closed at range of equivalence ratio (from 0.9 to 1.1), at this range the adiabatic flame temperature will be higher than others range (greater than 1500K) consequence the degree of dissociation will be higher and can be see the effect of dissociation in this range

as will be shown in figure (5). To show the effect heat of combustion on adiabatic flame temperature a figure (3) was plotted as a heat of combustion at same equivalence ratio (stoichiometry condition $\Phi=1$) for multi fuels, where the adiabatic flame temperature was proportioned with heat of combustion as in equation 18. In figure (3), can be noted that the heat of combustion variation for methane, ethane, propane and butane fuels with and without dissociation, the heat of combustion change with the dissociation occurs. Maximum values heat of combustion occurs without dissociate for all fuels while the minimum values

when the only CO₂ was dissociating. To understanding this phenomenon a figure (4) was plotted for methane fuel and others fuels has same behavior, where in figure (4,a) can be noted if the mole fraction of CO is increased the heat of combustion will be decreased, while invers effect of CO₂, due to some of chemical energy storage in a CO (

carbon monoxide can be oxidized as fuel) then the net unchained energy (heat of combustion) in this case(the carbon dioxied dissociate) will be lass than others. Also, in this figure, the heat of combustion will be increased when the mole fractins of CO₂, H₂ and OH are increased too, but it is decreased when the mole fraction of H₂O is increased.

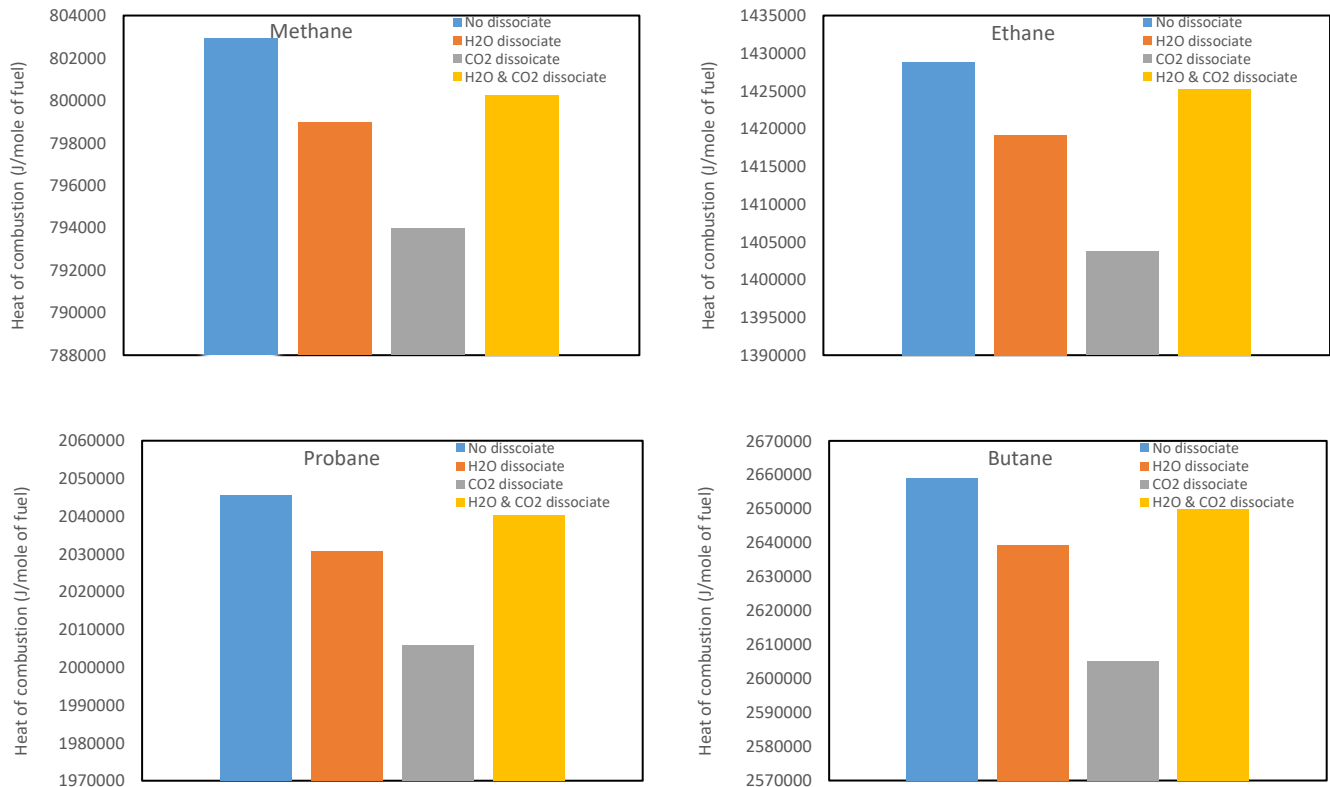


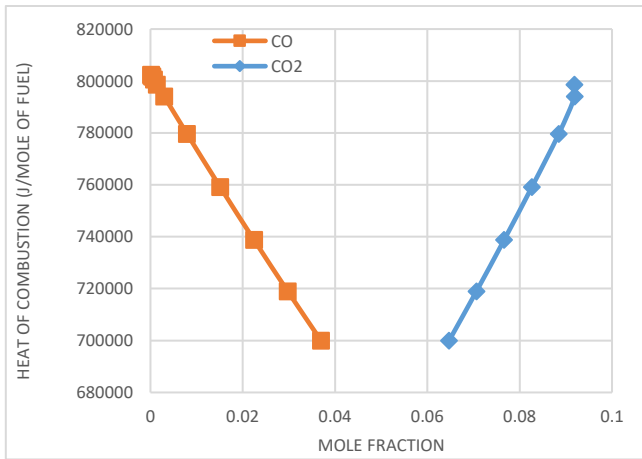
Figure (3) variation heat of combustion

In case of only H₂O is dissociation, the heat of combustion is greater than when only CO₂ is dissociation figure (3), this can be caused: if CO₂ is dissociating then mole fraction of CO₂ is decreasing that lead to heat of combustion will be decreased too as shown in figure (4,a). Additional, when the H₂O is dissociation perform to decreased the mole fraction of H₂O, as shown in figure (4,c), this caused increasing in heat of combustion, therfor the heat of combustion in case of only H₂O dissociation is greater than when only CO₂ is dissociation. By return to figure 3, the heat of combustion, when both H₂O and CO₂ are dissociating, is greater than

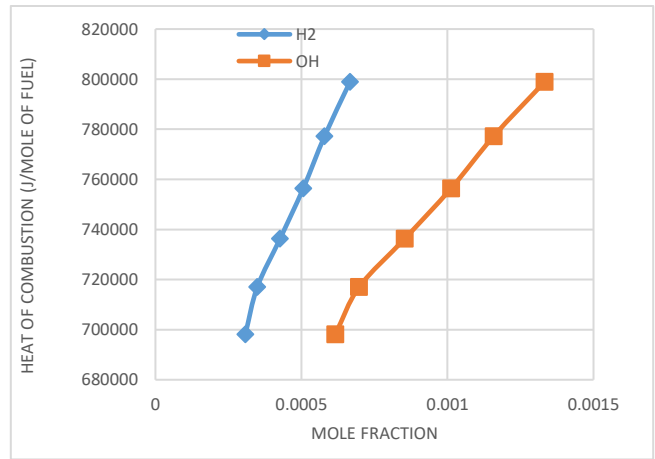
only H₂O or CO₂ is dissociating, that can be explains, for this case (both dissociation), dut to rducing mole fraction for H₂O and CO₂ together, by rducing the mole fraction of H₂O lead to increasing in heat of combustion as shown in figure 2,c comparino with only H₂O or CO₂ dissociating case. While rducing in mole fraction of CO₂ will be performed to decreasing in heat of combustion as shown in figure 2,a comparsion with no dissociation case. From demonstrate above can be considered amidst case between no dissociation and dissociating only H₂O or CO₂ case was occurred when both H₂O and CO₂ are dissoication

together. From the results explained in figures 3 and 4 can be told the bigger adiabatic flame temperature must be considered when no dissociation occurs and the smallest adiabatic flame temperature must be occurred with only CO₂ was dissociating, and relatively the adiabatic flame temperature, when both H₂O and CO₂ wear dissociation,

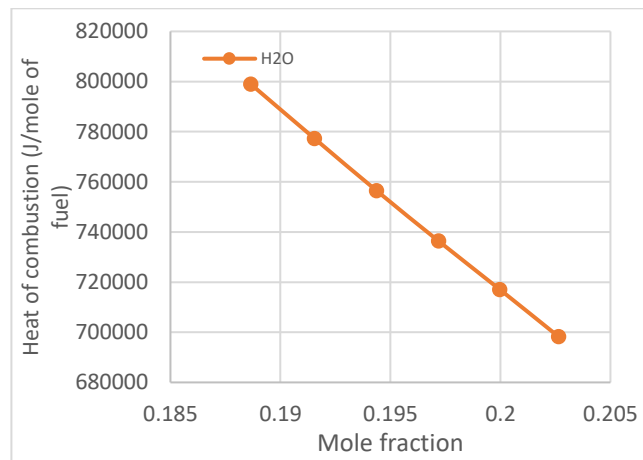
was higher than only H₂O or CO₂ was dissociation. This actuality can be seen clearly in figure (5). In this figure, for all fuels, can be shown the higher adiabatic flame temperature occurs when no dissociation case and the lower adiabatic flame temperature occurs when only CO₂ was dissociation.



(a)



(b)



(c)

Figure (4) variation of heat combustion with mole fraction for Methane fuel

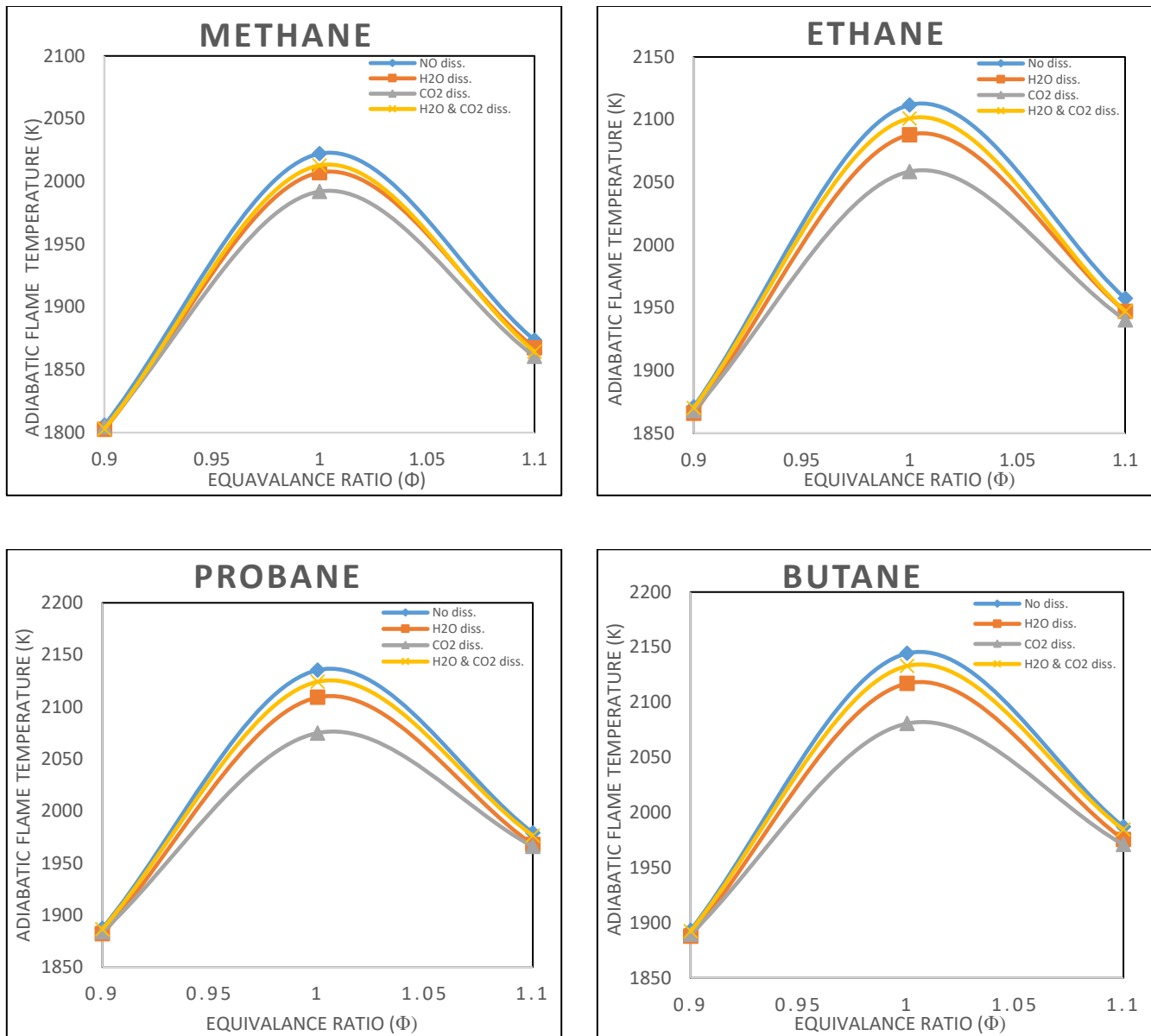


Figure (5) the effect of dissociate H₂O and CO₂ on adiabatic flame temperature.

Conclusion

To explore the effect of dissociation on adiabatic flame temperature a theoretical model was utilized in this study no dissociation, only H₂O dissociation, only CO₂ dissociation and both H₂O and CO₂ dissociation together. From the results shown above can be concluded the following:

With dissociation occurs the adiabatic flame temperature is decreasing.

The dissociation is significant at range of equivalence ratio (0.9 to 1.1) on adiabatic flame temperature.

The CO₂ has the bigger effect to reducing of adiabatic flame temperature comparative with only H₂O or both H₂O and CO₂ dissociation.

Symbol

Symbol	Definition	SI Units
a	Number mole of air	mole

b	Number mole of CO ₂ in products	=
c	Number mole of CO in products	=
cp	Specific heat at constant pressure	kJ/kg K
d	Number mole of H ₂ O in products	mole
f	Number mole of O ₂ in products	mole
h	Enthalpy	kJ/kg K
K _p	Equilibrium constant	
n	Number mole	mole
p	Pressure	N/m ²
Q	Heat of combustion	J/mole of fuel
T	Temperature	K
Greek symbols		
α	Amount dissociate from CO ₂ in products	mole
ε	Amount dissociate from H ₂ O in products	mole
φ	Equivalence ratio	
Subscribe		
adi	Adiabatic condition	
e	exiting combustion products	
i	Incoming fuel	
in	Initial	
o	Original	
p	Products	
R	Reactants	

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